

Data assimilation for prediction of ammonium in wastewater treatment plant: from physical to data driven models

Victor Bertret ^{1, 2, 3}, Roman Le Goff Latimier ², Valérie Monbet ³

¹Purecontrol, 68 Av. Sergent Maginot, Rennes, FRANCE victor.bertret@purecontrol.com

²Univ Rennes, ENS Rennes, IETR CNRS UMR 6164

³IRMAR, Université Rennes 1, CNRS, Rennes, FRANCE

28 March 2025



purecontrol

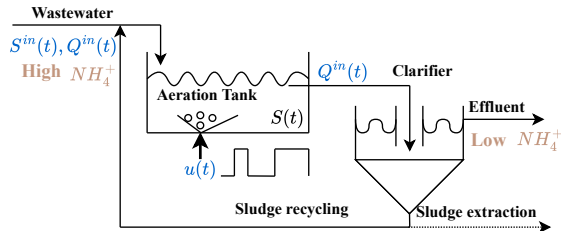


Outline

- 1 Wastewater Treatment Plants
- 2 Possible models for ammonium concentration
- 3 Model's calibration with data assimilation
- 4 Simulated Results
- 5 First real results

Alternated Activated Sludge Plants

Zoom on the secondary treatment of **Alternated Activated Sludge Plants (AAS)** :



- Municipal plants.
- **Input** : NH_4^+ (ammonium) high.
 - $Q^{in}(t)$, inflow.
 - $S^{in}(t)$, inlet concentration.
- **Output** : NH_4^+ low.

Objective : Reduce concentration of NH_4^+ coming from inlet water (nitrogen removal).

How? : By **controlling** the addition of oxygen in the aeration tank with $u(t)$.

Aeration control

The removal of nitrogen is carried out by alternating between :

- **Aeration phases** (energy-intensive) : oxygen is added using a compressor.
- **Non-aeration phases** : complete absence of oxygen.

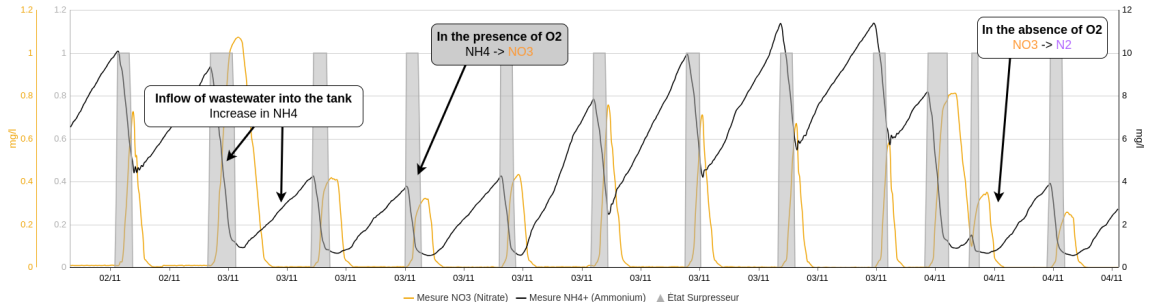


Figure – Nitrogen removal in the aeration tank.

Socio-economic Context

- **Increase** in environmental standards.
- Increase in **price** of energy.
- Increase in **variability** of energy.

Consequence : Minimize electric consumption.

Possible solution

Feedforward/Scheduling Control.



Condition

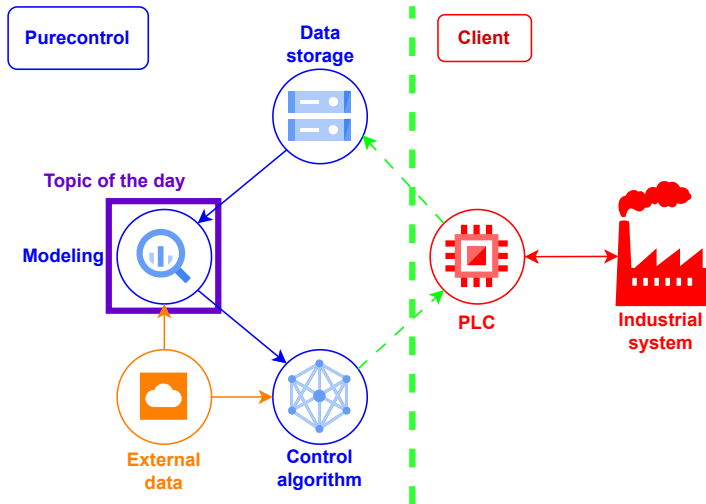
Dynamic model (NH_4^+).

Wastewater Treatment Plants

- **Complex** and **stochastic** system.
- **Expensive** and **unreliable** sensors.
- Controlled by **rudimentary** controllers.

Consequence : Finding new control algorithms.

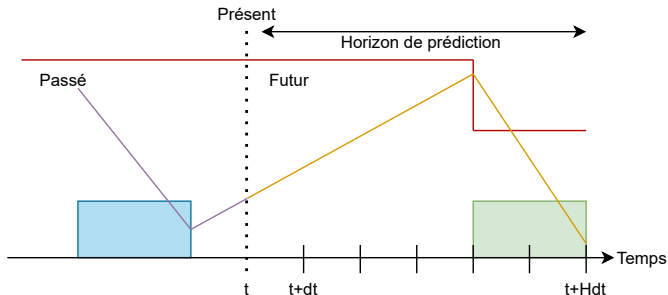
Purecontrol Solution for Energy Optimization



Model Predictive Control (MPC)

What is MPC ?

Model Predictive Control (MPC) predicts the system's future behavior using a dynamic model, allowing the generation of optimal control actions.



Recalculated at each time step $dt \Rightarrow$ **dynamic adaptation** to system variations.

Prediction Objective

24-hour stochastic prediction of ammonium (NH_4^+).



Modeling Requirements

Calibration of parameters and uncertainties.

Outline

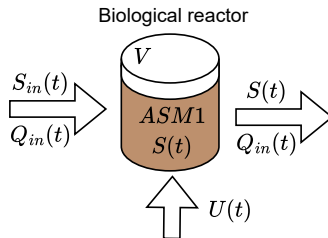
- 1 Wastewater Treatment Plants
- 2 Possible models for ammonium concentration
- 3 Model's calibration with data assimilation
- 4 Simulated Results
- 5 First real results

Well-known physic model

Development of family of **ASM's** physic based model

$$\frac{\partial S(t)}{\partial t} = \frac{Q^{in}(t)}{V} (S^{in}(t) - S(t)) + r(t, S(t), u(t))$$

- $S(t)$, **unknown** concentration of species.
- V , **unknown** volume of the reactor.
- $(Q^{in}(t), S^{in}(t))$, **known** inflow and inlet concentration.
- $u(t)$, **known** control applied to the system.



Our Case Study

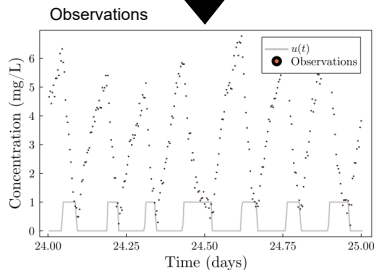
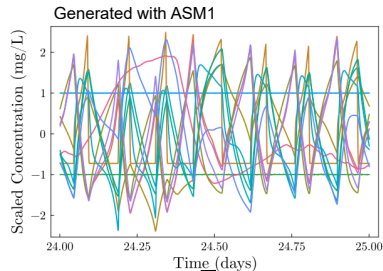
Main objective : High-precision NH_4^+ predictions over a 24-hour horizon.

Problem decomposition :

$$P(S(t), S_{in}(t)) = \overbrace{P(S(t)|S_{in}(t))}^{\text{NH}_4 \text{ Dynamics}} \times \overbrace{P(S_{in}(t))}^{\text{Inlet Estimation}}$$

System characteristics :

- Medium Dimensionality
- Strong Interactions & High Uncertainty
- Partial Observability



White-box model : Reduced ASM1 model

$$\frac{\partial S(t)}{\partial t} = \frac{Q^{in}(t)}{V} \left(\overbrace{S^{in}(t) - S(t)}^{\text{Not modified}} + \overbrace{r(t, S(t), u(t))}^{\text{Modified part}} \right)$$

• Problem :

- Complex physic model.
- 13 species.
- Many parameters.

• Solution : Reduced ASM1 Model

- 5 species
- Still 21 parameters.

Table 2 Process kinetics and stoichiometry for carbon oxidation, nitrification, and denitrification

Component	1	2	3	4	5	6	7	8	9	10	11	12	13	Process Rate, μ_i [$\text{ML}^{-1}\text{T}^{-1}$]
f Process	i	S_i	X_i	N_i	$X_{i,AS}$	$X_{i,AN}$	$A_{i,P}$	$S_{i,O}$	$S_{i,NO}$	$S_{i,NO}$	$S_{i,NO}$	$S_{i,NO}$	$S_{i,NO}$	
1 Aerobic growth of heterotrophs		$-\frac{1}{Y_H}$			1			$-\frac{1-Y_H}{Y_H}$		$-i_{NH}$			$-\frac{i_{NH}}{14}$	$\mu_H \left(\frac{S_H}{K_{S,H} + S_H} \right) \left(\frac{S_O}{K_{O,H} + S_O} \right) X_{H,H}$
2 Anaerobic growth of heterotrophs		$-\frac{1}{Y_H}$			1			$-\frac{1-Y_H}{2.86 Y_H}$	$-i_{NH}$				$-\frac{i_{NH}}{14 \cdot 2.86 Y_H}$	$\mu_H \left(\frac{S_H}{K_{S,H} + S_H} \right) \left(\frac{K_{O,H}}{K_{O,H} + S_O} \right) \cdot \left(\frac{S_{NO}}{K_{NO,H} + S_{NO}} \right) \eta_H X_{H,H}$
3 Aerobic growth of autotrophs						1		$-\frac{4.57 - Y_A}{Y_A}$	$\frac{1}{Y_A}$	$-i_{NH}$	$-\frac{1}{Y_A}$		$-\frac{i_{NH}}{14 \cdot Y_A}$	$\mu_A \left(\frac{S_{NO}}{K_{S,A} + S_{NO}} \right) \left(\frac{S_O}{K_{O,A} + S_O} \right) X_{A,A}$
4 Decay of heterotrophs			$1 - f_H$	-1			f_H					$i_{NH} - f_H i_{NH}$		$i_{NH} X_{H,H}$
5 Decay of autotrophs			$1 - f_A$	-1			f_A					$i_{NH} - f_A i_{NH}$		$i_{NH} X_{A,A}$
6 Ammonification of soluble organic nitrogen									1	-1			$\frac{1}{14}$	$k_d S_{NO} X_{H,H}$
7 Hydrolysis of entrapped organics	1			-1										$k_h \frac{X_H X_{H,H}}{K_H + (X_H X_{H,H})} \left[\left(\frac{S_H}{K_{S,H} + S_H} \right) + \eta_H \left(\frac{K_{O,H}}{K_{O,H} + S_O} \right) \left(\frac{S_{NO}}{K_{NO,H} + S_{NO}} \right) \right] X_{H,H}$
8 Hydrolysis of entrapped organic nitrogen										1	-1			$\mu_H (X_{NO} / X_H)$
Observed Conversion Rates [$\text{ML}^{-1}\text{T}^{-1}$]	$r_i = \sum_j \mu_j \nu_{ij}$													
Stoichiometric Parameters:														Kinetic Parameters:
Heterotrophic yield: Y_H														Heterotrophic growth and decay:
Aerobic yield: Y_A														$\mu_H, K_{S,H}, K_{O,H}, K_{NO,H}$
Mass N/Man COD in biomass: i_{NH}														Anaerobic growth and decay:
Mass N/Man COD in products from biomass: i_{NH}														$\mu_H, K_{S,H}, K_{O,H}, K_{NO,H}$
														Correction factor for aerobic growth of heterotrophs: η_H
														Ammonification: k_d
														Hydrolysis: k_h, K_H
														Correction factor for anaerobic hydrolysis: η_H

Figure – Matrix representation of the ASM1 model.

Grey-box Model : Focus on Ammonium

Simplified Physics-Based Model :

$$\frac{\partial S_{NH}(t)}{\partial t} = \underbrace{\frac{Q^{in}(t)}{V} [S_{NH}^{in}(t) - S_{NH}(t)]}_{\text{Not modified}} - \underbrace{\beta u(t) \frac{S_{NH}(t)}{S_{NH}(t) + K}}_{\text{Modified part}}$$

where V , β , and K are **unknown** parameters.

Key Remarks :

- **Simple** yet effective model.
- Few parameters, lacking direct **physical interpretation**.
- Based on multiple **assumptions** whose validity is **uncertain**.

Black-box Model : Linear State Space Model vs. Local Linear Regression

Linear State Space Model

$$S(t+1) = AS(t) + Bu(t) + CE(t) + \eta_t$$

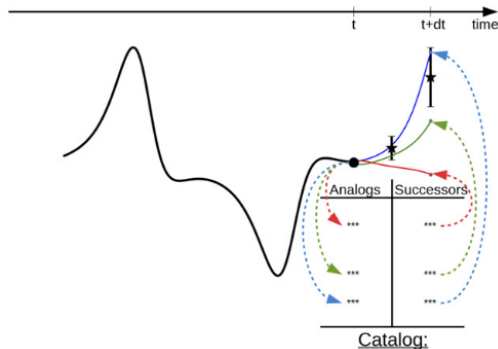
$$y(t) = HS(t) + \epsilon_t$$

Key Properties :

- **No physical meaning.**
- Assumes **global linearity**.
- Only based on **data-driven** methods.

Local Linear Regression

- Linear Regression on the k nearest neighbors.



Model Comparison

White-box

- **Based on physical laws.**
- **Requires many parameters** (often hard to estimate).
- Large number of species.
- High interpretability but may be too rigid.

Grey-box

- Uses simplified **mechanistic models** with data-driven corrections.
- **Reduces the number of parameters** compared to White-box.
- Trade-off between interpretability and flexibility.

Black-box

- **Fully data-driven.**
- Uses statistical or machine learning models.
- **No physical meaning**, purely empirical.
- Flexible but requires a lot of data and may lack generalization.

How to reconstruct the hidden concentrations and quantify the uncertainty ?

State Space Model structure

Separation of the model into two parts

- **Transition equation :**

$$S[t + h] = \text{ChosenModel}(S[t], U[t], E[t]) + \eta_t, \quad \eta_t \sim \mathcal{N}(0, \Sigma_\eta)$$

- **Observation equation :**

$$Y_{NH}[t] = H(S[t]) + \epsilon_t, \quad \epsilon_t \sim \mathcal{N}(0, \Sigma_\epsilon)$$

How can I find **jointly** the **hidden** variables, the **parameters** of the model and the **uncertainties** ?

Methods for Uncertainty Quantification and Latent Space Reconstruction

White-box

- **Main interest** : Latent states reconstruction using observers (Gernaey et al., 2004).
- **Parameter Estimation** : Often neglected due to model complexity (Chachuat, 2001).
- **Uncertainty Handling** : Rarely integrated directly ; relies on a posteriori sensitivity analysis (Boukroune, 2008).

Grey-box

- **Hybrid Calibration** : Combines mechanistic models with data-driven parameter tuning (Stare et al., 2006).
- **Uncertainty Handling** : Few models explicitly calibrate both parameters and uncertainty (Stentoft et al., 2018).
- **Key Challenge** : Ensuring consistency between physics-based and ML components.

Black-box

- **Fully Data-driven** : Requires large datasets ; lacks physical interpretability.
- **Uncertainty Estimation** : Difficult to quantify and integrate into assimilation frameworks (Alvi et al., 2023).
- **Recent Advances** : Local linear regression improves performance while reducing complexity (Chau et al., 2021).

Outline

- 1 Wastewater Treatment Plants
- 2 Possible models for ammonium concentration
- 3 Model's calibration with data assimilation**
- 4 Simulated Results
- 5 First real results

Grey-box calibration example

- **Transition equation :**

$$S_{NH}[t+h] = S_{NH}[t] + h \left[\frac{Q^{in}[t]}{V} [S_{NH}^{in}[t] - S_{NH}[t]] - \beta u[t] \frac{S_{NH}[t]}{S_{NH}[t] + K} \right] + w_t, \quad \eta_t \sim \mathcal{N}(0, \sigma_\eta^2)$$

- **Observation equation :**

$$Y_{NH}[t] = S_{NH}[t] + \epsilon_t, \quad \epsilon_t \sim \mathcal{N}(0, \sigma_\epsilon^2)$$

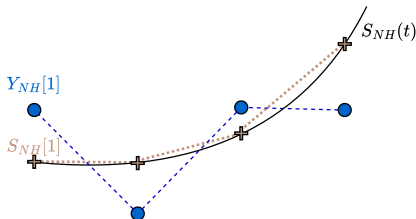
Majority of studies assume no observation noise during training.

Standard training : Prediction Error Minimization (PEM)

Training Dataset : $(Y_{NH}[i], \dots, Y_{NH}[N])$

Prediction Error Minimization : replace $S_{NH}[i]$ by observations $Y_{NH}[i]$

$$\min_{V, \beta, K} \sum_{t=1}^{N-1} \left[Y_{NH}[t+1] - \left(Y_{NH}[t] + h \left[\frac{Q^{in}[t]}{V} [S_{NH}^{in}[t] - Y_{NH}[t]] - \beta u[t] \frac{Y_{NH}[t]}{Y_{NH}[t] + K} \right] \right) \right]^2$$



How to **adapt** to **hidden** variables and **observation** noise ?

Data assimilation integrates real-world observations into models.

Key Challenges :

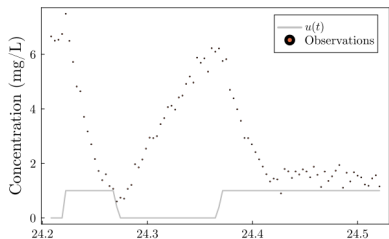
- **Reconstructing Hidden States :**

- **Sequential Methods :** More time-consuming but provide stronger theoretical guarantees.
- Variational Methods : Minimization of a cost function.

- **Calibrating Model Parameters and Uncertainties :**

- Direct Likelihood Maximization : Involves challenging steps such as differentiating over sequential methods (which can be unstable).
- Maximizing the complete likelihood with the **Expectation-Maximization** algorithm.

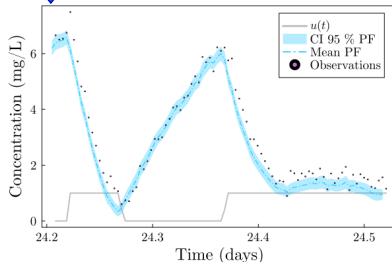
Filtering and Smoothing : Estimation of the latent variables



Filtering
or
Smoothing

$$p(S_{NH}[t] | Y_{NH}[1], \dots, Y_{NH}[t])$$

$$p(S_{NH}[t] | Y_{NH}[1], \dots, Y_{NH}[T])$$



Condition : Known parameters.

■ Linear model

- Kalman Filter and Smoother

■ Nonlinear model

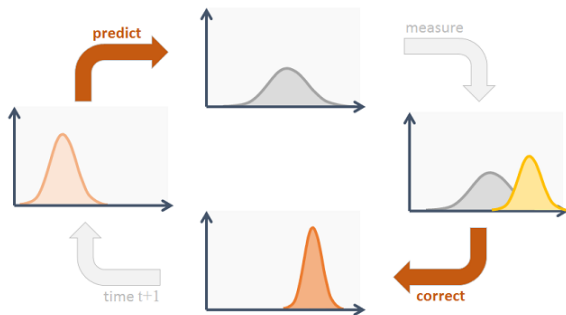
◇ Linearization

- Extended Kalman Filter and Smoother

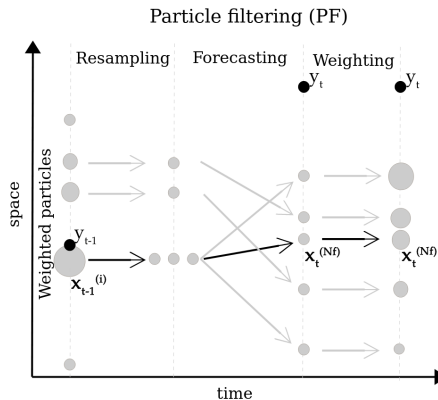
◇ Sequential Monte Carlo

- Ensemble Kalman Smoother and Filter
- Particle Filter and Backward Smoother

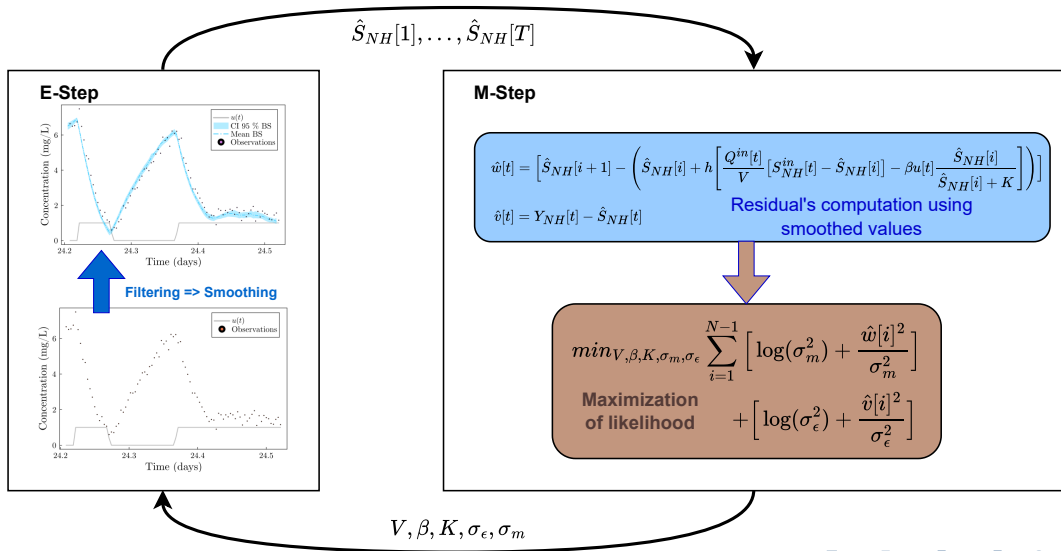
Kalman Filter



Particle Filter



Monte-Carlo Expectation Maximization (MCEM)



Outline

- 1 Wastewater Treatment Plants
- 2 Possible models for ammonium concentration
- 3 Model's calibration with data assimilation
- 4 Simulated Results**
- 5 First real results

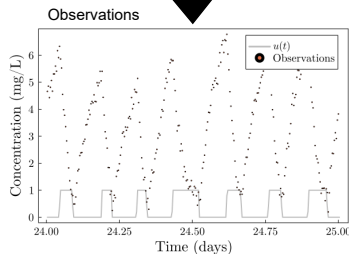
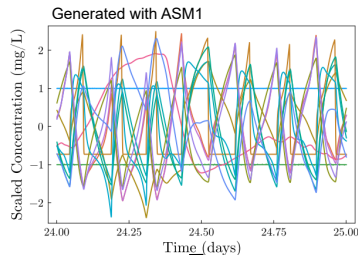
Experimental Setup

Objective :

- **Evaluate** model performance.
- Assess the **quality** of **uncertainty calibration**.

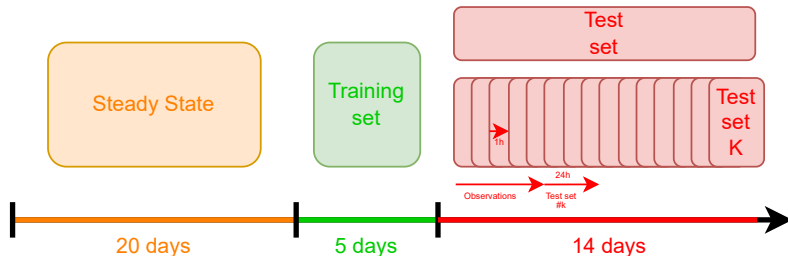
Experimental Design :

- Data generated from a simulator based on **ASM1**.
- ORP-based aeration control.
- **Diverse** external conditions.
- **Training** : 5 days | **Testing** : next 14 days.
- **Repeated** 10 times for each condition.



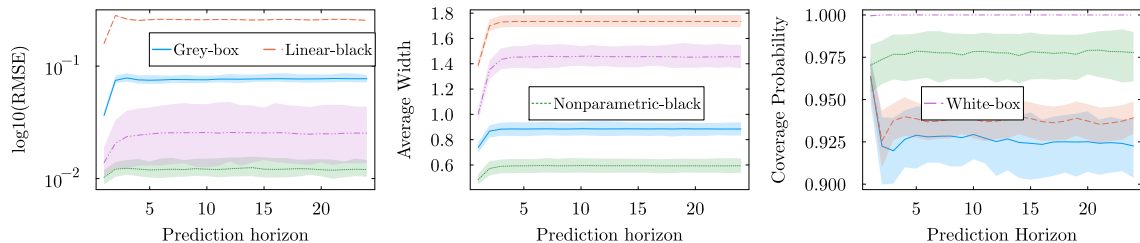
Metrics

New **observations** are assimilated **every hour**, and **24-hour predictions** are made.



- **Root Mean Squared Error (RMSE)** : Quantifies the average magnitude of errors between predicted and actual values.
- **Average Width (AW)** : Represents the mean width of prediction intervals.
- **Coverage Probability (CP)** : Measures the proportion of times the true value lies within the predicted interval.

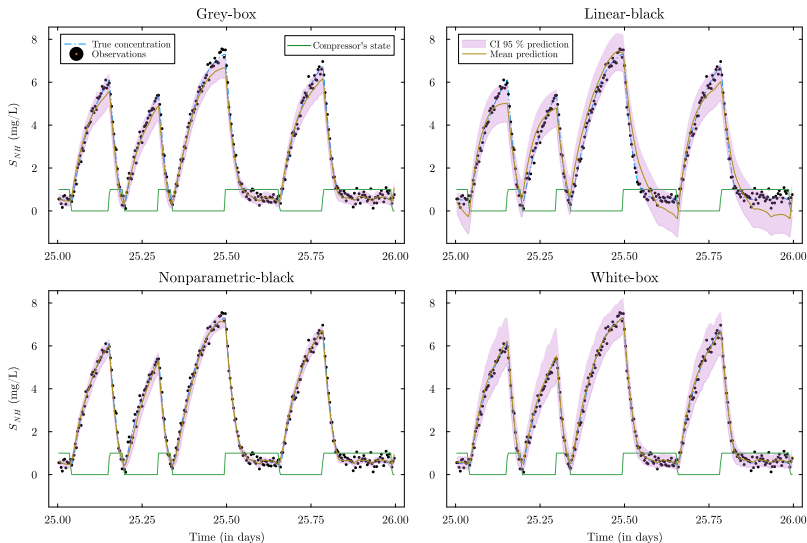
RMSE, AW, and CP Over Time Horizon



Key Observations :

- The **linear model** has the highest RMSE, while **LLR** achieves the best RMSE and AW.
- **White-box model** shows low RMSE but wide CI, indicating training instability.
- Most models are well-calibrated, except for the **white-box model**.

24h Model Predictions



Key Observations :

- **Linear model** fails to capture saturation at 0.
- **Grey-box model** shows bias at high concentrations.
- **White-box model** is well-calibrated but has wide confidence intervals.
- **LLR** achieves the best overall performance.

Estimated Parameters

Simulated observation standard deviation : 0.2 mg/L.

Model	Training Time (seconds)	Estimated Observation Standard Deviation	Estimated s_{NH} Standard Deviation
Grey-box	813	0.184	0.103
Linear Black-box	162	0.162	0.180
Nonparametric Black-box	3990	0.197	0.062
White-box	294000	0.189	0.109

Key Observations :

- All models provide accurate estimates of the observation standard deviation.
- **Linear model** is the fastest, while the **white-box** is extremely computationally expensive.
- **Nonparametric Black-box** achieves the lowest standard deviation for s_{NH} .



Grey-box Model

- **Balanced** performance according to simplifications.
- Slight bias in high ammonium concentrations.
- Low computational cost.

Black-box Model

- **Best RMSE and AW** and well-calibrated confidence intervals for LLR.
- Linear version lacks expressivity (fails to model saturation).

White-box Model

- **Low RMSE** but large uncertainty intervals.
- Computationally expensive (long training time).
- **Unstable** training.

Outline

- 1 Wastewater Treatment Plants
- 2 Possible models for ammonium concentration
- 3 Model's calibration with data assimilation
- 4 Simulated Results
- 5 First real results**

First Real-World Experiment

Experimental Setup :

- **Period** : April 12 – May 8, 2023.
- **Location** : Acigné, France.
- **Facility** : Wastewater treatment plant (14,000 PE).
- **Sampling Frequency** : Every minute.

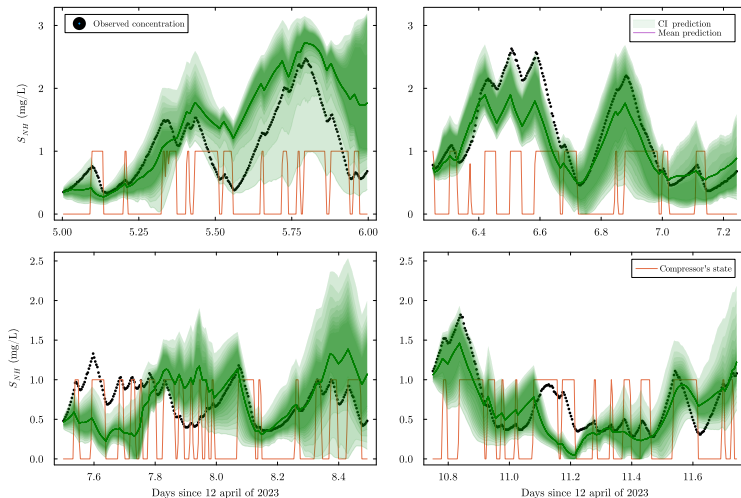
Available Data :

- **Inflow rate.**
- **Ammonium sensor measurements** (NH_4^+).
- **No direct inlet concentration data.**

Objective

Evaluate the performance of the non-parametric black-box model on real-world data.

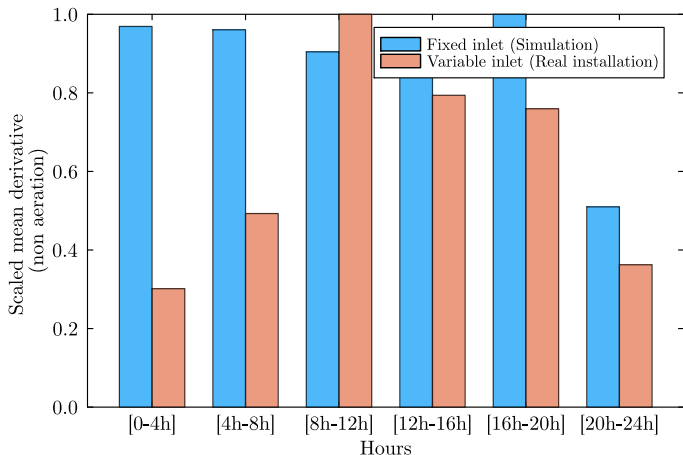
24h Model Predictions on Real Data



Key Observations :

- **Trend vs Amplitude :** Model struggles more with amplitude than trend.
- **Uncertainty Calibration :** Increased uncertainty, indicating good calibration.
- **Limitations :** Assumption of **constant inlet concentrations** is **violated** in real data.

Inlet Diurnal Variation in Catalog



Keys observations :

- **High Variability** : Significant fluctuations in the derivative within LLR catalogs.
- **Model Adjustment** : Need to incorporate **additional covariates** to improve performance.

- **Research Contributions :**

- **Comparison** of various model types for ammonium prediction within a **data assimilation** framework.
- The **non-parametric** black-box model outperformed all other models in terms of predictive **accuracy** and **uncertainty estimation**.
- General trends were captured in **real data**, but performance still **needs improvement**.

- **Research Perspectives :**

- Integration of heteroscedastic noise.
- Enhancement of LLR on real data using covariates (e.g., rain, time of day, etc.).
- Inlet concentration estimation.

Thank you for your attention
Questions ?

References I

- Alvi, M., Batstone, D., Mbamba, C. K., Keymer, P., French, T., Ward, A., Dwyer, J., and Cardell-Oliver, R. (2023). Deep learning in wastewater treatment : a critical review. *Water Research*, 245 :120518.
- Boukroune, B. (2008). *Estimation de l'état des systèmes non linéaires à temps discret. Application à une station d'épuration*. PhD thesis, Université Henri Poincaré - Nancy I.
- Chachuat, B. (2001). *Methodologie d'Optimisation Dynamique et de Commande Optimale des Petites Stations d'Epuration a Boues Activees*. PhD thesis, Institut National Polytechnique de Lorraine (INPL).
- Chau, T. T. T., Ailliot, P., and Monbet, V. (2021). An algorithm for non-parametric estimation in state–space models. *Computational Statistics & Data Analysis*, 153 :107062.
- Gernaey, K. V., van Loosdrecht, M. C., Henze, M., Lind, M., and Jørgensen, S. B. (2004). Activated sludge wastewater treatment plant modelling and simulation : state of the art. *Environmental Modelling and Software*, 19(9) :763–783.
- Stare, A., Hvala, N., and Vrečko, D. (2006). Modeling, identification, and validation of models for predictive ammonia control in a wastewater treatment plant—a case study. *ISA Transactions*, 45(2) :159–174.
- Stentoft, P. A., Munk-Nielsen, T., Vezzaro, L., Madsen, H., Mikkelsen, P. S., and Møller, J. K. (2018). Towards model predictive control : online predictions of ammonium and nitrate removal by using a stochastic asm. *Water Science and Technology*, 79(1) :51–62.